

Attachment II

Causal Analysis Report

Chevron Richmond Refinery
Reportable Flaring Events

August 5, 2019
Start-up of Hydrogen Plant Train 1
(S-4449)

Refinery Flare Event – Cause Investigation Report

1. Date on which the report was drafted: October 29, 2019

2. The refinery name and site number:

Refinery: Chevron Richmond Refinery
Refinery Site Number: A0010

3. The assigned refinery contact name and phone number:

Contact Name: Laura Kurt
Contact Phone Number: (510) 242-5219

Is this a rescission/modification of a previous report: No.

Date of initial report: N/A

Reason for rescission/modification: N/A

4. Identification of flare (s) at which the reportable event occurred by reviewing water seal monitoring data to determine which seals were breached during the event

Flare	Reportable Event (SO2 or Vent Gas Volume)
H2 (S-6021)*	Vent Gas Volume

**Note: The Hydrogen Plant (H2) flare does not have a water seal.*

5. The flaring event duration for each affected flare

Flare (Source Number): H2 (S-6021)

The Date(s) of the event: August 5, 2019

The start time of the event: 9:40AM on 8/5/2019

The end time of the event: 10:26PM on 8/5/2019

The net duration of event: 12 hours and 46 minutes

6. A brief description of the flaring event –

On August 5, 2019, at approximately 9:40AM, Operations introduced hydrocarbon feed to the Hydrogen Plant Train 1 (S-4449) as part of start-up procedures. Start-up procedures include routing flows, comprised mostly of hydrogen gas, to relief. The Hydrogen Plant does not have flare gas recovery or a water seal, and therefore all relief flow results in flaring. The vent gas volume exceeded 500,000 scf on August 5, 2019.

7. A process flow diagram showing the equipment and process units that were the primary cause of the event.

See Attachment IIa

8. The total volume of vent gas flared (MMSCF) throughout the event

Flare	Volume (MMSCF)
H2	24

9. The emissions associated with the flaring event per calendar day

Flare	Calendar Day	CH4 (lbs.)	NMHC (lbs.)	SO2 (lbs.)
H2	August 5, 2019	3614	278	0

Assumptions used to calculate emissions – consistent with the reporting under Reg. 12-11.

10. A statement as to whether or not the gas was scrubbed to eliminate or reduce any entrained compounds and a list of the compounds for which the scrubbing was performed.

The vent gas was not scrubbed to eliminate or reduce any entrained compounds.

11. The primary cause of the flaring event including a detailed description of the cause and all contributing factors. Also identify the upstream process units that contributed vent Gas flow to the flare header and provide other flow instrumentation data where available.

Flaring occurred during Train 1 start-up per procedure. Vent gas originated from the Hydrogen Plant Train 1 (S-4449) and associated equipment, including S-4471.

12. Describe all immediate corrective actions to stabilize the flaring event, and to reduce or eliminate emissions (flare gas recovered or stored to minimize flaring during the event). If a decision was made not to store or recover flare gas, explain why.

Operations used start-up procedures. The Hydrogen Plant does not have flare gas recovery.

13. Was the flaring the results of an emergency? If so, was the flaring necessary to prevent an accident, hazard or release to the atmosphere?

The flaring was not due to an Emergency (defined in Regulation 12-12-201) as interpreted by the BAAQMD.

14. If not the result of an emergency and necessary to prevent an accident, hazard or release to the atmosphere, was the flaring consistent with an approved FMP? If yes, provide a citation to the facility's FMP and any explanation necessary to understand the basis for this determination.

The flaring was consistent with Chevron's FMP Section 2.1 Table 2-4. Table 2-4 identifies the vent before PSA1 (S-4449) and PSA 1 as sources that may flare in non- emergency events (e.g. start-up, shutdown).

15. If the flaring was due to a regulatory mandate to vent to flare, why couldn't the gas be recovered, treated, and used as fuel gas?

N/A. Flaring was not due to regulatory mandate.

16. Identify and describe in detail each prevention measure (PM) considered to minimize flaring from the type of reportable flaring event that occurred.

a) State whether the PM is feasible (and will be implemented), or not feasible

b) Explain why the PM is not feasible, if applicable

Flaring cannot be prevented during plant start-up due to facility and relief system design.

Start-up of Hydrogen Plant Train 1

On August 5, 2019, at approximately 9:40AM, Operations introduced hydrocarbon feed to the Hydrogen Plant Train 1 (S-4449) as part of start-up procedures. Start-up procedures include routing flows, comprised mostly of hydrogen gas, to relief. The Hydrogen Plant does not have flare gas recovery or a water seal, and therefore all relief flow results in flaring. The vent gas volume exceeded 500,000 scf on August 5, 2019.

